

METHOD FOR REMOVING MERCURY IN EXHAUST GAS
AND SYSTEM THEREFOR

TECHNICAL FIELD

5 The present invention relates to a mercury removing method for removing mercury from exhaust gas of a boiler and a mercury removing system therefor. More particularly, it relates to a mercury removing method suitable for removing mercury contained in exhaust gas with a low Cl content
10 discharged from a coal-fired boiler or the like and a system for implementing the said method.

BACKGROUND ART

Conventionally, it has been thought that mercury
15 exists in exhaust gas in forms of metallic mercury insoluble in water and mercury chloride soluble in water. If metallic mercury can be converted to mercury chloride in the presence of a catalyst such as a denitrification catalyst, mercury can be removed by a desulfurization apparatus on the
20 downstream side (for example, see Japanese Patent Provisional Publication No. 10-230137 (No. 230137/1998)).

However, when mercury is converted to mercury chloride by using the denitrification catalyst, the conversion temperature is limited to 300 to 450°, so that in the case
25 of coal with a low Cl content, it is necessary to supply HCl

into exhaust gas to maintain the rate of conversion to mercury chloride, which presents problems of increased utility cost and occurrence of material corrosion.

On the other hand, a method can be thought of in which
5 a mercury oxidation catalyst is provided separately from the denitrification catalyst so that the conversion can be accomplished at a low temperature, and thereby metallic mercury is converted to mercury chloride in the presence of mercury oxidation catalyst.

10 However, when metallic mercury is converted to mercury chloride by using a mercury oxidation catalyst at a low temperature, excess NH₃ having been injected in an upstream denitrification apparatus flows down and adheres onto the catalyst as ammonium sulfate or acid ammonium sulfate, by
15 which the catalyst performance is sometimes deteriorated greatly. Also, there arises a problem in that the catalyst itself is closed by the adherend. Specifically, in an ammonia denitrification apparatus applied to a combustion boiler, ammonia (NH₃) is injected through an injection
20 nozzle in the combustion boiler or on the downstream side thereof to be allowed to react reductively with nitrogen oxides (NO, NO₂), by which a process for decomposing nitrogen oxides into nitrogen (N₂) and water (H₂O) is carried out. Ammonia added excessively in this process
25 exists in the exhaust gas and flows down to the downstream

side of the denitrification catalyst, and thereby produces ammonium sulfate or acid ammonium sulfate.

On the other hand, even when either of the denitrification or mercury oxidation catalysts is used, the 5 coexistence of NH₃ hinders a mercury oxidation reaction and hence causes an increase in the filling amount of catalyst.

DISCLOSURE OF THE INVENTION

In view of the above problems, the inventors conducted 10 studies earnestly to develop a method for removing mercury in exhaust gas, in which even if NH₃ leaks to the downstream side of the denitrification apparatus, hindrance to reaction due to NH₃ in mercury oxidation treatment can be avoided and the amount of catalyst can be decreased by enhanced catalyst 15 durability, and adhesion of ammonium sulfate to heating means such as an air heater and a heat exchanger such as a GGH can be prevented.

As a result, the inventors found that the above-described problems can be solved by combining an NH₃ 20 decomposition catalyst for decomposing NH₃ flowing down from the outlet of the denitrification apparatus with a mercury oxidation catalyst for oxidizing mercury into mercury chloride, which is provided on the downstream side of the NH₃ decomposition catalyst. The present invention was 25 completed from this point of view.

Accordingly, an object of the present invention is to provide a system for removing mercury in exhaust gas, in which mercury is removed from exhaust gas of a coal-fired boiler, wherein between a denitrification apparatus and a 5 wet type desulfurization apparatus, an NH₃ decomposition catalyst for decomposing NH₃ flowing down from the outlet of the denitrification apparatus and a mercury oxidation catalyst for oxidizing mercury into mercury chloride on the downstream side of the NH₃ decomposition catalyst are provided, and mercury having been oxidized into mercury 10 chloride is removed by the wet type desulfurization apparatus.

In the present invention, a mode can preferably be cited in which in the mercury removing system in which 15 heating means and a heat exchanger are provided between the denitrification apparatus and wet type desulfurization apparatus, the mercury oxidation catalyst is installed at least at one location of: between the downstream side of the NH₃ decomposition catalyst and the upstream of the heating 20 means; between the downstream side of the heating means and the upstream of the heat exchanger; and between the downstream side of the heat exchanger and the upstream side of the wet type desulfurization apparatus. It is preferable 25 that the mercury oxidation catalyst be a catalyst in which at least one kind selected from the group consisting of TiO₂,

SiO_2 , ZrO_2 , Al_2O_3 and zeolite is used as a carrier, and at least one kind selected from the group consisting of Pt, Ru, Rh, Pd, Ir, V, W, Mo, Ni, Co, Fe, Cr, Cu and Mn is carried on the carrier as an active component. Also, it is

5 preferable that the NH_3 decomposition catalyst be a catalyst in which at least one kind selected from the group consisting of TiO_2 , SiO_2 , ZrO_2 , Al_2O_3 and zeolite is used as a carrier, and at least one kind selected from the group consisting of Pt, Ru, Rh, Pd, Ir, V, W, Mo, Ni, Co, Fe, Cr,

10 Cu and Mn is carried on the carrier as an active component.

Also, another object of the present invention is to provide a method for removing mercury in exhaust gas, in which mercury is removed from exhaust gas of a coal-fired boiler, wherein the mercury removing method includes an NH_3

15 decomposition process for decomposing NH_3 flowing down from a denitrification process and a mercury oxidation process for oxidizing mercury into mercury chloride on the downstream side of the NH_3 decomposition process, which are provided between the denitrification process and a wet

20 desulfurization process, and mercury having been oxidized into mercury chloride is removed in the wet desulfurization process.

In the present invention, a mode can preferably be cited in which in the mercury removing method including a

25 heating process and a heat recovery process, which are

provided between the denitrification process and wet desulfurization process, the NH₃ decomposition process is carried out in a temperature zone of 300 to 450°C on the downstream side of the denitrification process, and the 5 mercury oxidation process is carried out at least in one location of: a temperature zone of 300 to 450°C on the downstream side of the NH₃ decomposition process; a temperature zone of 120 to 200°C on the downstream side of the heating process; or a temperature zone of 60 to 120°C on 10 the downstream side of the heat recovery process. When the mercury oxidation process is carried out on the downstream side of the heating process, the temperature can be controlled to a predetermined temperature in the range of 60 to 200°C. Also, the temperature in the mercury oxidation 15 process can be controlled by measuring the concentration of metallic mercury or mercury chloride in an oxidation catalyst outlet gas in the mercury oxidation process. Further, it is preferable that in the NH₃ decomposition process, NH₃ be treated so that the concentration of NH₃ at 20 the outlet is 1 ppm or lower, preferably 0.1 ppm or lower, and then mercury be oxidized in the mercury oxidation process.

According to the present invention, after NH₃ leaking to the downstream side of the denitrification catalyst has 25 been decomposed, mercury is oxidized, by which the hindrance

to reaction due to NH₃ can be avoided, and the amount of catalyst can be decreased by the increase in catalyst performance. Also, when the mercury oxidation catalyst is installed in a temperature zone behind the heating means such as the air heater, ammonium sulfate can be prevented from adhering, so that the amount of catalyst can be decreased by enhanced durability.

Also, by decomposing NH₃ leaking to the downstream side of the denitrification catalyst, ammonium sulfate can be prevented from adhering to the heating means such as the air heater or the heat exchanger such as the GGH, and further the durability of system can be enhanced by the decrease in frequency of soot blow.

Hereunder, an embodiment of the present invention will be described in detail, but the scope of the present invention is not limited by this embodiment.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 is a schematic view showing one example of a system for removing mercury in exhaust gas in accordance with the present invention;

Figure 2 is a flowchart showing a procedure flow for studying the installation location of a mercury oxidation catalyst in the mercury removing system in accordance with the present invention;

Figure 3 is a schematic explanatory view of an apparatus for removing mercury in exhaust gas which is used in example 1; and

5 Figure 4 is a schematic explanatory view of an apparatus for removing mercury in exhaust gas which is used in example 2;

In the above figures, reference numeral 1 denotes a boiler, 2 denotes a denitrification apparatus, 3 and 11 each denote an NH₃ decomposition catalyst, 4 denotes an air 10 heater (A/H), 5 denotes a dust collector, 6 denotes heat recovery side heat exchanger (GGH), 7 denotes a desulfurization absorption tower (wet type desulfurization apparatus), 8 denotes a reheating side heat exchanger (GGH), 9 denotes a stack, 10 and 12 each denote a mercury oxidation 15 catalyst, 13 denotes a reactor, 14 denotes an electric heater, 15 denotes a cooler, and 16 and 17 each denote a reactor.

BEST MODE FOR CARRYING OUT THE INVENTION

20 Method for removing mercury in exhaust gas

In a method for removing mercury in exhaust gas in accordance with the present invention, exhaust gas discharged from a coal-fired boiler is sent to a denitrification catalyst, and a denitrification process is 25 carried out. In the denitrification process, ammonia (NH₃)

is added as a reducing agent on the upstream side of the denitrification catalyst. Therefore, added excess NH₃ is contained in large amounts in the exhaust gas having been subjected to denitrification treatment. This NH₃ hinders
5 mercury oxidation reaction (mercury oxidation process) on the downstream side, and also adheres onto a catalyst as ammonium sulfate or acid ammonium sulfate when a low-temperature mercury oxidation catalyst is used. Therefore, the catalyst performance is deteriorated greatly, and the
10 adherend may close the catalyst.

For this reason, in the present invention, NH₃ that hinders the mercury oxidation reaction (mercury oxidation process) is removed from exhaust gas flowing down from the denitrification process on the upstream side of the mercury
15 oxidation catalyst. For this purpose, an NH₃ decomposition catalyst is installed just behind the denitrification catalyst. Excess NH₃ having been sent from the denitrification catalyst to the downstream side is decomposed on the NH₃ decomposition catalyst, and is removed
20 from the exhaust gas.

Next, in the present invention, mercury is removed from the exhaust gas from which NH₃ has been removed through the NH₃ decomposition process. For this purpose, first, mercury in the exhaust gas is subjected to oxidation
25 reaction with hydrogen chloride contained in large amounts

in the exhaust gas in the presence of the mercury oxidation catalyst in a mercury oxidation process, by which mercury is converted to mercury chloride. Then, the exhaust gas containing mercury chloride is caused to pass through a 5 downstream wet type desulfurization apparatus, by which mercury components in the exhaust gas are absorbed by an alkali absorbing solution used in a wet type desulfurization process and are removed.

Between the above-described denitrification process 10 and wet type desulfurization process, a heating process using a heater or steam and a heat recovery process using a gas heater are included. In such a system, the NH₃ decomposition process is carried out in a temperature zone of 300 to 450°C on the downstream side of the 15 denitrification process. The mercury oxidation process is carried out in any temperature zone of a temperature zone of 300 to 450°C on the downstream side of the NH₃ decomposition process, a temperature zone of 120 to 200°C on the downstream side of the heating process, and a temperature 20 zone of 60 to 120°C on the downstream side of the heat recovery process.

When the mercury oxidation process is carried out on the downstream side of the heating process, the temperature is preferably controlled to a predetermined temperature in 25 the range of 60 to 200°C. Also, the temperature in the

mercury oxidation process can be controlled by measuring the concentration of metallic mercury or mercury chloride in an oxidation catalyst outlet gas in the mercury oxidation process. Further, it is preferable that in the NH₃ decomposition process, NH₃ be treated so that the concentration of NH₃ at the outlet is usually 1 ppm or lower, preferably 0.1 ppm or lower, and then mercury be oxidized in the mercury oxidation process.

System for removing mercury in exhaust gas

Figure 1 shows one example of a system using the above-described method. A specific embodiment of the mercury removing system in accordance with the present invention will now be described in detail with reference to the accompanying drawings.

In the present invention, exhaust gas of a coal-fired boiler, which contains mercury (Hg), is caused to pass through the NH₃ decomposition catalyst, and then metallic mercury is oxidized into mercury chloride in the presence of the mercury oxidation catalyst. After metallic mercury is converted to water-soluble mercury chloride by the mercury oxidation catalyst on the upstream side of the wet type desulfurization apparatus, the exhaust gas is introduced into the desulfurization absorption tower, where desulfurization is accomplished by the alkali absorbing solution of the wet type desulfurization apparatus on the

downstream side. By this treatment, SO_x is absorbed and removed by bringing the exhaust gas into contact with the absorbing solution such as a lime slurry circulating solution in the desulfurization absorption tower within the system. At the same time, mercury chloride (HgCl₂) is dissolved in the absorbing solution and is removed.

In the system shown in Figure 1, on the downstream side of a boiler 1, a denitrification apparatus (SCR) 2, an NH₃ decomposition catalyst 3, an air heater (A/H) 4, which is heating means, a dust collector 5, a heat exchanger (GGH) 6 for recovering heat energy, a desulfurization absorption tower (wet type desulfurization apparatus) 7, a heat exchanger (GGH) 8 for reheating, and a stack 9 are arranged in that order. A mercury oxidation catalyst 10 is installed at any one location of: between the downstream side of the NH₃ decomposition catalyst 3 and the upstream side of the air heater (A/H) 4; between the downstream side of the air heater (A/H) 4 and the upstream side of the dust collector 5; and between the downstream side of the heat exchanger (GGH) 6 and on the upstream side of the desulfurization absorption tower (wet type desulfurization apparatus) 7.

In one example of the denitrification apparatus 2 used in this system, reducing agent injecting means is provided on the exhaust gas inflow side of the denitrification catalyst. As the reducing agent injecting means, means that

is made up of a reducing agent injection pipe and a plurality of spray nozzles is used. As a method for injecting a reducing agent including ammonia, there is available, for example, a method in which a reducing agent
5 is vaporized, and is diluted by adding air, inert gas, water vapor, etc. to the vaporized reducing agent before injection is accomplished. At this time, it is effective to arrange the nozzles so that the reducing agent flows uniformly in the catalyst layer, and in some cases, the nozzles are
10 arranged in the direction perpendicular to the gas flow.

Also, as the denitrification catalyst layer, a honeycomb-shaped catalyst, a catalyst layer formed by lapping the honeycomb-shaped catalysts, a catalyst layer formed by packing granular catalysts, or the like is used.

15 As the denitrification catalyst, a catalyst in which an active metal of at least one kind selected from a group consisting of V, W and Mo is contained in a carrier of TiO₂ or TiO₂ + SiO₂ composite oxide can be used. Also, a catalyst in which an active metal of at least one kind selected from
20 a group consisting of Pt, Pd, Ir, Ru, Cu, Co, Fe, Ag, Mn, Ni, Zn and In is contained in a carrier of at least one kind selected from a group consisting of Al₂O₃, SiO₂, ZrO₂, TiO₂, metallocsilicate, and zeolite can be used.

As the active metal, noble metals of Pt, Pd, Ru, Ir,
25 etc. are preferable. In particular, Pt-based metals are

preferable. Also, as the carrier, metallosilicate, ZSM5, silicalite, Y-type zeolite, mordenite, alumina, silica, titania, etc. can be used preferably. Although the shape of catalyst is not subject to any special restriction, a 5 honeycomb shape is preferable. The necessary amount of catalyst is usually in the range of 1000 to 50,000 h⁻¹ in terms of GHSV.

On the downstream side of the denitrification apparatus (SCR), the NH₃ decomposition catalyst 3 is 10 provided.

As the NH₃ decomposition catalyst 3 used in the present invention, a catalyst in which at least one kind selected from a group consisting of TiO₂, SiO₂, ZrO₂, Al₂O₃ and zeolite is used as a carrier, and at least one kind 15 selected from a group consisting of Pt, Ru, Rh, Pd, Ir, V, W, Mo, Ni, Co, Fe, Cr, Cu and Mn is carried on the carrier as an active component can be cited. From the viewpoint of durability against sulfur oxides contained in exhaust gas, as the carrier, in particular, titanium oxides or silicon 20 oxides are preferably used, and a catalyst in which a composite oxide containing TiO₂ or SiO₂ is used as a carrier and an oxide of vanadium, tungsten, molybdenum, or the like is carried as active metal species has a high activity.

In this embodiment, the mercury oxidation catalyst 10a, 25 10b or 10c is installed at one location of any of: between

the downstream side of the NH₃ decomposition catalyst 3 and the upstream side of the air heater 4 (10a) (temperature zone of 300 to 450°C); between the downstream side of the air heater 4 and the upstream side of the dust collector 5 (10b) (temperature zone of 120 to 200°C); or between the downstream side of the heat recovering heat exchanger 6 and the upstream side of the wet type desulfurization apparatus 7 (10c) (temperature zone of 60 to 120°C).

As the mercury oxidation catalyst 10 used in the present invention, a catalyst in which at least one kind selected from a group consisting of TiO₂, SiO₂, ZrO₂, Al₂O₃ and zeolite is used as a carrier, and at least one kind selected from a group consisting of Pt, Ru, Rh, Pd, Ir, V, W, Mo, Ni, Co, Fe, Cr, Cu and Mn is carried on the carrier as an active component can be cited. Like the NH₃ decomposition catalyst 3, from the viewpoint of durability against sulfur oxides contained in exhaust gas, as the carrier, in particular, titanium oxides or silicon oxides or composite oxides thereof are preferably used, and a catalyst in which a composite oxide containing TiO₂ or SiO₂ is used as a carrier and an oxide of vanadium, tungsten, molybdenum, or the like is carried as active metal species has a high activity.

In the present invention, in order to increase the specific surface area and solid acid amount of catalysts 3

and 10, Ti oxides that are rendered a composite oxide can be used as the carrier. As a metal forming the composite oxide of Ti, for example, silicon (Si), zirconium (Zr), aluminum (Al), and tungsten (W) can be cited. For example, composite 5 oxides of Ti and Si, Ti and Zr, Ti and Al, Ti and W, etc. can be used. Because none of these composite oxides form a sulfate easily, they can maintain a stable structure, so that the specific surface area and solid acid amount can be increased. Also, as necessary, a composite oxide of three-10 component system such as Ti and Si + Zr, Ti and Si + W, Ti and Si + Al, Ti and Zr + Al, and Ti and Zr + W can be used.

In the catalysts 3 and 10 of the present invention, at least one kind selected from a group consisting of Pt, Ru, Rh, Pd, Ir, V, W, Mo, Ni, Co, Fe, Cr, Cu and Mn is used as 15 an active component by being carried on the above-described carrier. Any of these catalysts has oxidation capability, and thus can oxidize metallic mercury into mercury chloride when it is used as the mercury oxidation catalyst 10.

The composition ratio of catalyst used in the present 20 invention is not subject to any special restriction. As one example, with respect to 100 parts by weight of a carrier consisting of one kind of an oxide or a composite oxide, for an active component of a base metal element such as V, W, Mo, Ni, Co, Fe, Cr, Cu and Mn, a composition of 0.5 to 20 parts 25 by weight as an oxide thereof can preferably be cited, and

for an active component of a noble metal element such as Pt,
Ru, Rh, Pd, and Ir, a composition of 0.01 to 1 part by
weight as a metal thereof can preferably be cited. More
specifically, in the case of the mercury oxidation catalyst
5 10, with respect to 100 parts by weight of TiO₂-SiO₂
composite oxide carrier, a composition with an active
component of 1.2 parts by weight of vanadium pentoxide and 9
parts by weight of tungsten oxide (WO₃), a composition of
0.05 part by weight of Pt and 9 parts by weight of tungsten
10 oxide (WO₃), and the like compositions can be cited. Also,
in the case of the NH₃ decomposition catalyst 3, with
respect to 100 parts by weight of TiO₂ carrier, a
composition with an active component of 4 to 10 parts by
weight of vanadium pentoxide, a composition of 0.5 part by
15 weight of Pt, 0.6 part by weight of vanadium pentoxide, and
9 parts by weight of tungsten oxide (WO₃), and the like
compositions can be cited.

Also, for the above-described catalysts used in the
present invention, an arbitrary shape can be selected
20 according to the system configuration. Any integrally
molded shape such as a pellet shape, plate shape,
cylindrical shape, corrugated shape, or honeycomb shape can
be used.

In this system shown in Figure 1, on the downstream
25 side of the NH₃ decomposition catalyst 3, the air heater

(A/H) 4, which is heating means, and the dust collector 5 are provided. The dust collector 5 is not subject to any special restriction, and may be of any type that can collect dust roughly before exhaust gas is introduced into the 5 desulfurization absorption tower 7. On the downstream side of the dust collector 5, the heat exchanger (GGH) 6 for recovering heat energy is provided, and successively the desulfurization absorption tower (wet type desulfurization apparatus) 7 is provided. The desulfurization absorption 10 tower 7 is not subject to any special restriction, and a wet type desulfurization apparatus that is generally used for flue gas treatment or a desulfurization apparatus in which a cooling tower is provided on the upstream side of an absorption tower can be used. As the absorbing solution 15 used for wet desulfurization, an aqueous solution (alkali absorbing solution) of an absorbent such as calcium carbonate, calcium oxide, calcium hydroxide, sodium carbonate, and sodium hydroxide can be cited.

In this system using the wet desulfurization method, 20 on the downstream side of the desulfurization absorption tower 7, the heat exchanger 8 for reheating is provided, and exhaust gas is discharged to the air from the stack 9 after passing through these apparatuses. In the heat exchanger 8 for reheating, combustion exhaust gas whose temperature has 25 been decreased is heated by heat energy recovered by the

heat exchanger 6 for recovering heat provided on the upstream side of the desulfurization absorption tower 7. When combustion exhaust gas is discharged, the gas after being purified is heated and turned to a high-temperature 5 gas, and the high-temperature gas is discharged. For this purpose, the heat exchanger 8 for supplying heat is provided on the downstream side of the wet type desulfurization apparatus 7.

The heat exchanger 6 for recovering heat and the heat 10 exchanger 8 for reheating each are formed by a gas heater of a system in which heat energy is exchanged with a heat medium being used as a medium. The heat exchangers 6 and 8 may be of a type in which the exhaust gas is cooled and heated, respectively, and may be a separate system or a gas-15 gas heater in which heat exchange is accomplished directly.

In the above-described system shown in Figure 1, metallic mercury is removed as described below.

In the exhaust gas from the boiler 1, a Cl content in fuel such as coal exists as HCl, and metallic mercury (Hg) 20 is oxidized into mercury chloride ($HgCl_2$) on the mercury oxidation catalyst 10. In the desulfurization absorption tower 7, SO_2 in the exhaust gas is removed, and at the same time $HgCl_2$ is removed. Since the concentration of HCl in the exhaust gas is overwhelmingly higher than the 25 concentration of Hg, excess HCl is contained. However, the

excess HCl is absorbed by the alkali aqueous solution such as milk of lime in the desulfurization absorption tower 7, so that it is not discharged from the stack. The exhaust gas from which Hg has been removed in the desulfurization 5 absorption tower 7 is introduced into the heat exchanger 8 for reheating, being heated by heat energy recovered by the heat exchanger 6, and is discharged from the stack 9.

As described above, in the present invention, mercury is oxidized in the presence of the mercury oxidation 10 catalyst, and mercury in the exhaust gas, which has been converted to water-soluble mercury chloride, is removed in the wet desulfurization process. On the other hand, the optimum temperature for oxidation of mercury changes according to the Cl content in fuel, so that a too high or 15 too low temperature may cause metallic mercury to be discharged without being sufficiently oxidized.

To avoid this problem, in this embodiment, the mercury oxidation catalyst 10 is installed at any one location of: between the downstream side of the NH₃ decomposition 20 catalyst 3 and the upstream side of the air heater 4 (10a) (temperature zone of 300 to 450°C); between the downstream side of the air heater 4 and the upstream side of the dust collector 5 (10b) (temperature zone of 120 to 200°C); or between the downstream side of the heat recovering heat 25 exchanger 6 and the upstream side of the wet type

desulfurization apparatus 7 (10c) (temperature zone of 60 to 120°C).

Figure 2 is a flowchart showing a procedure for studying the installation location of the mercury oxidation catalyst.

The exhaust gas to be treated in the present invention is a boiler exhaust gas of a thermal electric power station, factory, etc. in which fuel containing sulfur and mercury, such as coal or heavy oil, is burned, or a heating furnace exhaust gas of a metal factory, refinery, petrochemical plant, etc., so that it contains carbon dioxide, oxygen, SO_x, smoke and soot, and water, and has a large discharge amount. The following is a description of a preferred mode for treating the exhaust gas of coal-fired boiler.

Firstly, when coal of medium- and high-concentration (not lower than 0.01%) Cl is used, with coal of low-concentration (not higher than 0.01%) Cl not being used, the mercury oxidation catalyst 10 is installed in the temperature zone of the denitrification catalyst 2 on the downstream side of the NH₃ decomposition catalyst 3 and on the upstream side of the air heater 4 (10a) (temperature zone of 300 to 450°C). In this mode, since the mercury oxidation catalyst 10 is used at a high temperature, the amount of catalyst can be decreased.

Secondly, when coal of low-concentration Cl is used,

the mercury oxidation catalyst 10 is installed in a temperature zone of 60 to 200°C on the downstream side of the heating process using the air heater 4 or the like. The installation location is changed depending on whether or not 5 a system in which ammonia is injected is used in the dust collector 5. The reason for this is that if ammonia is injected into the exhaust gas, the concentration of ammonia in the exhaust gas, which has been decreased by the NH₃ decomposition catalyst, increases again, which hinders the 10 mercury oxidation reaction caused by the mercury oxidation catalyst 10, and hence decreases the efficiency of conversion to mercury chloride.

Therefore, in the system in which ammonia is injected in the dust collector 5, the mercury oxidation catalyst 10 15 is installed at a location on the upstream side of the dust collector 5 and on the downstream side of the air heater 4 (10b) (temperature zone of 120 to 200°C), where ammonia is not injected into the exhaust gas.

On the other hand, in the system in which ammonia is 20 not injected in the dust collector 5, the mercury oxidation catalyst 10 is installed at a location which is on the downstream side of the dust collector 5, on the downstream side of the heat recovering heat exchanger 6, and on the upstream side of the wet type desulfurization apparatus 7 25 (10c) (temperature zone of 60 to 120°C). In this mode,

since ammonia is not injected, the catalyst can be installed either before or behind the dust collector 5. However, on the downstream side of the dust collector 5, smoke and soot in the exhaust gas have been removed, so that gas 5 penetration apertures of catalyst can be decreased, which achieves the effect of being able to decrease the amount of catalyst.

For the mercury oxidation catalyst for exhaust gas shown in Figure 1, by installing the mercury oxidation 10 catalyst at the optimum location which has each temperature zone in accordance with the flow shown in Figure 2, the metallic mercury in combustion exhaust gas can effectively be oxidized into mercury chloride capable of being absorbed and removed by the desulfurization absorption tower 7.

15 Also, according to this system, by measuring the concentration of metallic mercury or mercury chloride in the gas at the outlet of the mercury oxidation catalyst 10, the mercury oxidation process is controlled so as to have a proper temperature. Thereby, even without adding a 20 chlorinating agent (HCl etc.), metallic mercury can be oxidized into mercury chloride stably according to the Cl content in the exhaust gas, so that the metallic mercury in the exhaust gas can be removed effectively.

As described above, according to the system of the 25 present invention, after NH₃ leaking to the downstream side

of the denitrification catalyst has been decomposed, mercury is oxidized, by which the hindrance to reaction due to NH₃ can be avoided, and the amount of catalyst can be decreased by the increase in catalyst performance. Also, when the 5 mercury oxidation catalyst is installed in a temperature zone behind the heating means such as the air heater, ammonium sulfate can be prevented from adhering, so that the amount of catalyst can be decreased by enhanced durability.

Also, by decomposing NH₃ leaking to the downstream 10 side of the denitrification catalyst, ammonium sulfate can be prevented from adhering to the heating means such as the air heater or the heat exchanger such as a GGH, and further the durability of system can be enhanced by the decrease in frequency of soot blow.

15 The following experiments were conducted to verify the effect of removing mercury in the present invention, but the present invention is not restricted by the description of these examples.

20

EXAMPLES

Example 1

A test was carried out to evaluate the oxidation rate of mercury and the decomposition rate of ammonia by using an apparatus for removing mercury in exhaust gas which is shown 25 in Figure 3.

In the apparatus of this example 1, H₂O, CO₂, O₂, NH₃ and HCl were added to N₂ gas, and the vapor of metallic mercury was mixed to prepare a simulation gas. The simulation gas was introduced into a reactor 13, and was
5 allowed to pass through an NH₃ decomposition catalyst 11 and a mercury oxidation catalyst 12 provided in the reactor 13. For the catalysts, the temperature thereof was controlled by an electric heater 14. An inlet gas, an outlet gas of the NH₃ decomposition catalyst 11, and an outlet gas of the
10 mercury oxidation catalyst 12 were sampled.

The test conditions were as described below: the content of added gases were H₂O : 7%, CO₂ : 12%, O₂ : 5%, NH₃ : 10 ppm, and HCl : 10 ppm, the mercury concentration was Hg : 30 µg/m³N, the reactor temperature was 350°C at
15 ordinary pressure, the NH₃ decomposition catalyst SV was 6000 h⁻¹, the mercury oxidation catalyst SV was 6000 h⁻¹, the NH₃ decomposition catalyst was V₂O₅/TiO₂-SiO₂, and the mercury oxidation catalyst was V₂O₅-WO₃/TiO₂-SiO₂. Table 1 gives the test results.

[Table 1]

Catalyst No.	Inlet	NH ₃ decomposition catalyst outlet	Mercury oxidation catalyst outlet
ToHg concentration ($\mu\text{g}/\text{m}^3\text{N}$)	30	30	30
HgCl ₂ concentration ($\mu\text{g}/\text{m}^3\text{N}$)	0.5	5.2	28.8
HCl concentration (ppm)	10	-	-
NH ₃ concentration (ppm)	10	<0.1	<0.1
NH ₃ decomposition rate (%)	-	>99.9	-
Hg oxidation rate (%)	-	15.9	95.2

From the test results given in Table 1, it was found
 5 that by decomposing 99% or more of ammonia by the NH₃
 decomposition catalyst, 95% or more of metallic mercury in
 the gas can be oxidized, and can be removed by the
 downstream wet type desulfurization apparatus.

By this example, it was made clear that in the above-
 10 described embodiment, when the mercury oxidation catalyst 10
 is installed just behind the NH₃ decomposition catalyst 3
 and on the upstream side of the air heater 4 (10a)
 (temperature zone of 300 to 450°C), mercury oxidation
 reaction proceeds sufficiently.

Example 2

A test was carried out to evaluate the oxidation rate of mercury and the decomposition rate of ammonia by using an apparatus for removing mercury in exhaust gas which is shown 5 in Figure 4.

In the apparatus of this example 2 as well, H₂O, CO₂, O₂, NH₃ and HCl were added to N₂ gas, and the vapor of metallic mercury was mixed to prepare a simulation gas. The simulation gas was first introduced into a reactor 16, and 10 was allowed to pass through the NH₃ decomposition catalyst 11 provided in the reactor 16, and the temperature of the catalyst was controlled by the electric heater 14. The gas coming out of the reactor 16 passed through a cooler 15, and then was introduced into a next reactor 17. The gas was 15 allowed to pass through the mercury oxidation catalyst 12 provided in the reactor 17, and the temperature of the catalyst was controlled by the electric heater 14. An inlet gas, an outlet gas of the NH₃ decomposition catalyst 11, and an outlet gas of the mercury oxidation catalyst 12 were 20 sampled.

The test conditions were as described below: the content of added gases were H₂O : 7%, CO₂ : 12%, O₂ : 5%, NH₃ : 10 ppm, and HCl : 10 ppm, the mercury concentration was Hg : 30 µg/m³N, the temperature of NH₃ decomposition catalyst was 350°C and that of mercury oxidation catalyst 25

was 160°C at ordinary pressure, the NH₃ decomposition catalyst SV was 6000 h⁻¹, the mercury oxidation catalyst SV was 6000 h⁻¹, the NH₃ decomposition catalyst was V₂O₅/TiO₂-SiO₂, and the mercury oxidation catalyst was V₂O₅-WO₃/TiO₂-SiO₂. Table 2 gives the test results.

[Table 2]

Catalyst No.	Inlet	NH ₃ decomposition catalyst outlet	Mercury oxidation catalyst outlet
ToHg concentration ($\mu\text{g}/\text{m}^3\text{N}$)	30	30	30
HgCl ₂ concentration ($\mu\text{g}/\text{m}^3\text{N}$)	0.5	5.2	28.8
HCl concentration (ppm)	10	-	-
NH ₃ concentration (ppm)	10	<0.1	<0.1
NH ₃ decomposition rate (%)	-	>99.9	-
Hg oxidation rate (%)	-	15.9	95.2

From the test results given in Table 2, it was found
10 that by decomposing 99% or more of ammonia by the NH₃ decomposition catalyst, even if the temperature of the mercury oxidation catalyst is as low as 160°C, 95% or more of metallic mercury in the gas can be oxidized, and can be removed by the downstream wet type desulfurization apparatus.

By this example, it was made clear that in the above-described embodiment, when the mercury oxidation catalyst 10 is installed in a temperature zone of 60 to 200°C (10b, 10c) on the downstream side of the heating process using the air 5 heater 4 etc., mercury oxidation reaction proceeds sufficiently.

The above is a description of the embodiment and examples of the present invention. These embodiment and examples are provided to make the understanding of the 10 present invention easy, and do not limit the claims of the present invention.